

# Solving Partial Differential Algebraic Equations and reactive transport models

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## 1 Introduction

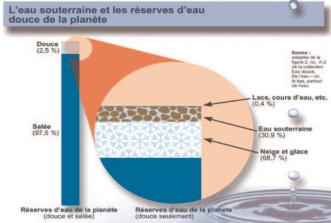
- 1 Introduction
- 2 Physical model

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## Water resources



Pictures: Yves Chaux, Rennes, France

Diagram: [http://www.ec.gc.ca/water/f\\_main.html](http://www.ec.gc.ca/water/f_main.html)

## Reactive transport modeling

- Coupling transport by advection-dispersion with geochemistry
- System of Partial Differential Algebraic equations
- Model with thermodynamic equilibrium
- Method of lines: first discretize in space then in time  $\Rightarrow$  DAE system
- Explicit scheme (SNIA): decoupling but stability restrictions
- Implicit scheme (Global): stability but nonlinear coupled system

### Our method: global approach GDAE



S. Krättele, P. Knabner, (2005); A new numerical reduction scheme for fully coupled multicomponent transport-reaction problems in porous media; Water Resources Research, Vol. 41, W09414, 17 pp.



S. Molins, J. Carrera, C. Ayora, Carlos and M.W. Saaltink, (2004); A formulation for decoupling components in reactive transport problems; Water Resources Research, Vol.40, W10301, 13 pp.



C. de Dieuleveult, J. Erhel, M. Kern; A global strategy for solving reactive transport equations; Journal of Computational Physics, 2009



## Mass action laws

### Aqueous reactions

$$x_i(c) = K_{ci} \prod_{j=1}^{N_c} c_j^{S_{ij}}, \quad i = 1, \dots, N_x \quad (1)$$

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$$y_i(c, s) = K_{si} \prod_{j=1}^{N_c} c_j^{A_{ij}} \prod_{j=1}^{N_s} s_j^{B_{ij}}, \quad i = 1, \dots, N_y, \quad (2)$$

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### Precipitation reactions

$$\Pi_i(c) = K_{pi} \prod_{j=1}^{N_c} c_j^{E_{ij}}, \quad i = 1, \dots, N_p \quad (3)$$

## Mass conservation laws

### Chemical variables and functions

$$X = \begin{pmatrix} c \\ s \\ p \end{pmatrix}, \quad \Phi(X) = \begin{pmatrix} c + S^T x(c) + A^T y(c, s) + E^T p \\ s + B^T y(c, s) \\ \Pi(c) \end{pmatrix} \quad (4)$$

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### Chemical model

$$\begin{cases} \Phi(X) = \begin{pmatrix} T \\ W \\ 1 \end{pmatrix}, \\ c \geq 0, \\ s \geq 0, \\ p > 0. \end{cases} \quad (5)$$

## Transport model

### Advection-Dispersion operator

$$\mathcal{L}(u) = \nabla \cdot (vu - D\nabla u)$$

$$D = d_m I + \alpha_T \|v\| I + (\alpha_L - \alpha_T) \frac{vv^T}{\|v\|}$$

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### Transport of mobile species

$$C(X) = c + S^T x(c) \quad (6)$$

$$\omega \frac{\partial T_i}{\partial t} + \mathcal{L}(C_i) = Q_i, \quad i = 1, \dots, N_c \quad (7)$$

with boundary and initial conditions

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### Space discretization

with (for example) a finite difference method

$$T = (T_1, \dots, T_{N_m}) \quad (8)$$



## Coupling transport with chemistry

### Semi-discrete reactive transport model

$$\left\{ \begin{array}{l} \omega \frac{dT_i}{dt} + LC_i(X) = Q_i + G_i, \quad i = 1, \dots, N_c, \\ \Phi(X_j) - \begin{pmatrix} T_j \\ W_j \\ 1 \end{pmatrix} = 0 \quad j = 1, \dots, N_m, \\ \text{initial condition for } T, \end{array} \right. \quad (9)$$

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### DAE formulation

$$\left\{ \begin{array}{l} \omega \frac{d\text{vec } T}{dt} + (L \otimes I)\text{vec } C(X) - \text{vec } Q - \text{vec } G = 0, \quad i = 1, \dots, N_c, \\ \text{vec } \Phi(X) - (I \otimes N)\text{vec } T - \text{vec } F = 0 \end{array} \right. \quad (10)$$

## DAE Global approach with substitution

Time discretization: BDF scheme

$$\frac{d\text{vec } T}{dt} \simeq \frac{a}{\Delta t} \text{vec } T + \frac{1}{\Delta t} \text{vec } Z,$$
$$\begin{cases} \frac{a\omega}{\Delta t} \text{vec } T + (L \otimes I) \text{vec } C(X) - \dots = 0, \\ -(I \otimes N) \text{vec } T + \text{vec } \Phi(X) - \dots = 0, \end{cases}$$

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Substitution

$$R(X) = \frac{\Delta t}{a\omega} (L \otimes N) \text{vec } C(X) + \text{vec } \Phi(X) - \dots$$

The Jacobian of  $R$  is

$$J_R(X) = \frac{\Delta t}{a\omega} (L \otimes N) \text{diag} \left( \frac{dC}{dX}(X_j) \right) + \text{diag}(J_\Phi(X_j)).$$

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Nonlinear system

$$R(X) = 0$$

solved with Newton method

## GRT3D software

### Transport modules

- The velocity  $v$  is computed with MODFLOW
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- The derivatives  $J_\Phi(X)$  and  $dC(X)/dX$

### Coupling modules

- The function  $R(X)$
- The derivative  $J_R(X)$
- The DAE solver IDA in SUNDIALS using Newton-LU method
- The sparse linear solver UMFPACK



## Versions of GRT3D

First version with logarithms

No elimination of  $T$  and  $C$

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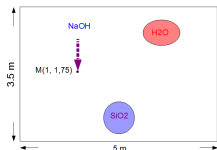
### Optimized version without logarithms

Elimination of  $T$  and  $C$  in the linearized equations

## Numerical experiment

### Andra qualification test

Injection of alkaline water  $NaOH$  in a porous medium with quartz  $SiO_2$

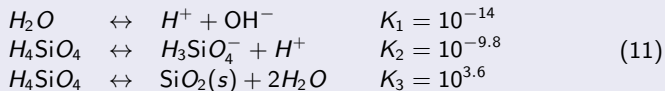


$$\left\{ \begin{array}{l} \epsilon = 1. \\ v = \begin{pmatrix} 5.7 \cdot 10^{-7} \\ 0. \end{pmatrix} \text{ m.s}^{-1} \\ d_m = 0 \\ \alpha_L = 0.2 \text{ m} \\ \alpha_T = 0.05 \text{ m} \\ T = 30 \text{ days} \\ \text{no flux boundary conditions} \end{array} \right.$$



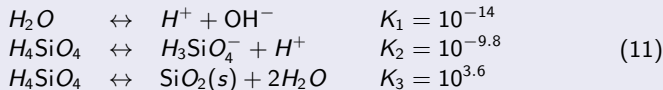
## Chemistry conditions

### Chemistry equations



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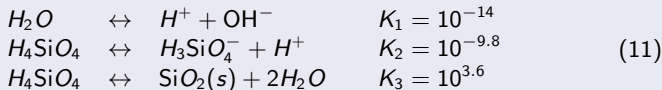


### Stoichiometric coefficients

	$Na^+$	$OH^-$	$H_4SiO_4$
$H^+$	0	-1	0
$H_3SiO_4^-$	0	1	1
$SiO_2$	0	0	1

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### Initial values

	$Na^+$	$OH^-$	$SiO_2$
Outside $M$	0	0	10.
At $M$	$10^{-2}$	$10^{-2}$	10.

## Accuracy results

### Accuracy of computed pH

$$E_{H^+} = \|\tilde{x}_{H^+} - x_{H^+}\|$$

Mesh	first GRT3D	reduced GRT3D	optimized GRT3D
21x14	1.333005E-11	1.591450E-11	8.040057E-11
41x28	2.489791E-09	2.489787E-09	8.113751E-11
81x56	7.640456E-09	7.640825E-09	3.055914E-10
71x101	7.747011E-09	7.746415E-09	4.161827E-10
161x112	7.9736E-09	7.9738E-09	2.6672E-10
322x224	-	3.0871E-09	4.3067E-10



## Performance results

### CPU time of GRT3D

Computations done on two six-core Intel Xeon processors X5690, with a frequency of 3.46 GHz and 4GB of RAM per core.

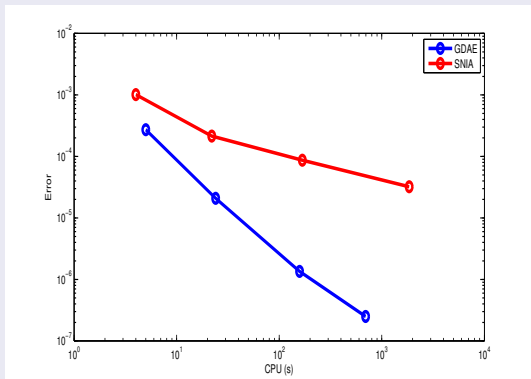
Mesh	first GRT3D	reduced GRT3D	optimized GRT3D
21x14	18 s	4 s	2 s
48x28	1 min 36 s	21 s	8s
81x56	6 min 33 s	1 min 53 s	50 s
71x101	11 min 55 s	3 min 28 s	1 min 21 s
161x112	32 min 43 s	16 min 30 s	4 min 32 s
322x224	-	1 h 52 min	37 min 38 s

## Comparison results

### Performance/Accuracy results

Comparison with an analytical solution

$$E_{Na^+} = \left[ \frac{1}{N_m N_t} \sum_{n,j} (\tilde{x}_{Na^+}(m_j, t_n) - x_{Na^+}(m_j, t_n)) \right]^{1/2}$$



## Conclusion

### Summary

- The DAE global approach (implicit scheme and Newton method) is very efficient
- Substitution is very efficient
- The model without logarithms is more efficient than with logarithms

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### Future work

- Precipitation-dissolution with vanishing  $p$
- Parallel computations